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High production of fatty alcohols in *Escherichia coli* with fatty acid starvation

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Abstract

Background: Microbial biofuel synthesis attracting increasing attention. Great advances have been made in producing fatty alcohols from fatty acyl-CoAs and fatty acids in *Escherichia coli*. However, the low titers and limited knowledge regarding the basic characteristics of fatty alcohols, such as location and toxicity, have hampered large-scale industrialization. Further research is still needed.

Results: In this study, we designed a novel and efficient strategy to enhance fatty alcohol production by inducing fatty acid starvation. We report the first use of deletions of acyl-ACP thioesterases to enhance fatty alcohol production. Transcriptional analysis was conducted to investigate the mechanism of the designed strategy. Then, fatty alcohol production was further enhanced by deletion of genes from competing pathways. Fatty alcohols were shown to be extracellular products with low toxicity. The final strain, *E. coli* MGL2, produced fatty alcohols at the remarkable level of 6.33 g/L under fed-batch fermentation, representing the highest reported titer of fatty alcohols produced by microorganisms.

Conclusions: Deletions of genes responsible for synthesis of fatty acids and competing products are promising strategies for fatty alcohol production. Our investigation of the location and toxicity of fatty alcohols suggest bright future for fatty alcohol production in *E. coli*.

Keywords: Escherichia coli, Fatty alcohols, Acyl-ACP thioesterases, Fatty acid starvation

Background

The increasing demand and limited supply of fuels has given rise to concern regarding prospects for sustainable development [1, 2]. Microbial production of high-energy fuels has emerged as a viable alternative to conventional fuels [3, 4]. Fatty acids and their derivatives are of particular interest owing to their high caloric value [5]. *Escherichia coli* is suitable for this purpose, not only because fatty acid metabolism in *E. coli* is well understand [6] but also because genetic techniques for *E. coli* have been extensively investigated [7, 8]. In the past decade, significant efforts have been

made to produce fatty acids, alcohols and alkanes in E. $coli\ [5,\ 9-13]$. Among those chemicals, fatty alcohols have attracted increasing attention because they can be widely used in medicines, cosmetics, detergents and skin care products [14].

Fatty alcohols can be produced from fatty acyl-ACPs, fatty acyl-CoAs, or fatty acids through the catalysis of fatty acyl reductase (*FAR*) [12, 15–17]. Great advances have been made in engineering microorganisms to produce fatty alcohols from fatty acyl-CoAs [5, 16] and fatty acids [17]. Three main strategies have been applied in these studies. First, a variety of fatty acyl reductases from marine bacteria, soil bacteria and plants have been expressed in *E. coli* to facilitate fatty alcohol production [16–19]. Second, genes related to fatty alcohol synthesis have been overexpressed [20]. Third, genes responsible for fatty alcohol degradation have been knocked out [18]. However, the highest reported titers of even

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and odd-chain fatty alcohols are only 3.78 and 1.9 g/L, respectively [20, 21], still far below levels suitable for industrialization.

In this study, a novel strategy was developed to enhance fatty alcohol production by inducing fatty acid starvation. Cellular location and toxicity studies of fatty alcohols are a crucial step that must occur before future industrialization. However, to our knowledge, no previous research has addressed these issues performed on these. Therefore, investigations on toxicity and the cellular localization of fatty alcohols were conducted.

Results and discussion

Enhancing fatty alcohol production via inducing fatty acid starvation

Fatty acids are a crucial component of all living organisms [22]. If the concentration of fatty acids drops, resulting in fatty acid starvation, the expression levels of genes for fatty acid synthesis are upregulated to satisfy growth needs. This process eventually leads to the accumulation of fatty acyl-ACPs, which are reduced to fatty alcohols by *FAR* (Fig. 1). There are various ways to block fatty acid formation, such as the mutation of *accD* (a subunit of acetyl-CoA carboxylase) [23]. In this study, acyl-ACP thioesterases rather than upstream genes were deleted to block fatty acid formation and to enhance fatty alcohol

production (Fig. 1). There are three reported acyl-ACP thioesterases in E. coli: tesA, tesB [24] and tesC [25]. In a subcellular localization analysis using Cell-PLoc 2.0, tesA, tesB and tesC were predicted to be located in the periplasm, inner membrane and cytoplasm, and cytoplasm, respectively [26]. Because fatty acids are synthesized in the cytoplasm in E. coli, tesC may play a key role in producing fatty acids. Moreover, it has been reported that the Michaelis constants (km) of tesA and tesB for native palmitoyl-ACP are 100 to 200 pM, which are over more than tenfold higher than those for palmitoyl-CoA [24]. These finding sugggest that tesA and tesB do not play major roles in producing fatty acids. Therefore, deletions of tesC, tesB and tesA were performed individually (Table 1). The fermentation results supported our presumption that the deletion of tesC would dramatically affect growth rate, fatty acid production and fatty alcohol production, whereas the effects of *tesB* and *tesA* deletions were less significant (Fig. 2a-c).

Subsequently, *tesB* and *tesA* were deleted sequentially from the MGKC strain to enhance fatty alcohol production. The growth curves of the engineered strains (MGKC, MGKCB and MGKCBA) are shown in Fig. 2d. Interestingly, although the growth rates decreased after thioesterase deletions, the final cell densities of the engineered strains were similar. Beyond our expectations,

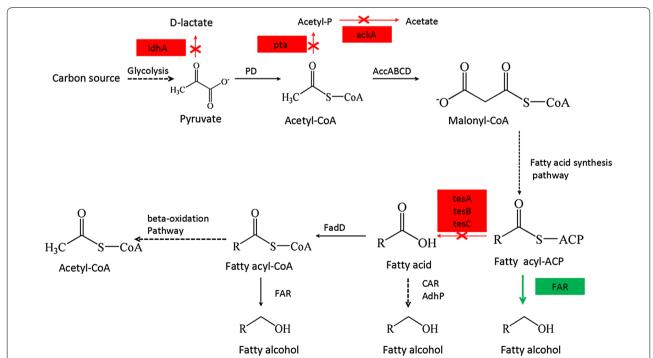


Fig. 1 Engineered pathway for fatty alcohol production in *E. coli*. The fatty alcohol synthesis flux from fatty acyl-ACP was enhanced by deletion of acyl-CoA thioesterases coupled with overexpression of fatty acyl-ACP reductase (*FAR*, *green line*). Competing pathways were blocked (*red line*) by deletion of lactic dehydrogenase (*IdhA*), phosphate acetyltransferase (*pta*) and acetate kinase (*ackA*)

Table 1 Plasmids and strains used in this study

Plasmids/strains	Relevant characteristic(s)	Reference/source	
Plasmids			
pMD [™] 18-T Vector	T-easy vector	Takara	
pTrcHisA	Expression vector	Invitrogen	
pKD46	Bla γβexo temperature conditional pSC101 replicon	[8]	
pEASY-cat-sacB	T-easy vector with cat-sacB cassette	Lab collection	
pL1	pTrcHisA containing the M. aquaeolei FAR gene	This study	
Strains			
W	E. coli K-12 MG1655	Lab collection	
MGKC	E. coli K-12 MG1655 ΔtesC	This study	
MGKB	E. coli K-12 MG1655 ΔtesB	This study	
MGKA	E. coli K-12 MG1655 ΔtesA	This study	
MGKCB	E. coli K-12 MG1655 ΔtesC ΔtesB	This study	
MGKCBA	E. coli K-12 MG1655 ΔtesC ΔtesB ΔtesA	This study	
MGL1	E. coli K-12 MG1655 ΔtesC ΔtesB ΔldhA::kan Δpta ΔackA	This study	
W/pL1	W bearing pL1	This study	
MGKC/pL1	MGKC bearing pL1	This study	
MGKB/pL1	MGKB bearing pL1	This study	
MGKA/pL1	MGKA bearing pL1	This study	
MGKCB/pL1	MGKCB bearing pL1	This study	
MGKCBA/pL1	MGKCBA bearing pL1	This study	
MGL2	MGL1 bearing pL1	This study	

after all three yet known fatty acyl-ACP thioesterases were knocked out, the E. coli still survived. Other thioesterases in *E. coli*, such as *ybhC* (acyl-CoA thioesterase) and paal (hydroxyphenylacetyl-CoA thioesterase), might possibly serve anaplerotic functions. The amounts of fatty alcohols and fatty acids produced in wild-type and engineered strains with FAR expression (W/pL1, MGKC/ pL1, MGKCB/pL1 and MGKCBA/pL1) are shown in Fig. 2e, f. W represents the E. coli K-12 MG1655 wildtype strain in this study. The highest production of fatty alcohols and fatty acids in strains W/pL1, MGKC/pL1 and MGKCB/pL1 was observed 24 h after inoculation, whereas for strain MGKCBA/pL1, production peaked after 36 h. The fatty alcohol titer increased from 480 to 710 mg/L as a result of the deletion of tesC, whereas, fatty acid production decreased from 30 to 15 mg/L. Similarly, the fatty alcohol titer increased to 750 mg/L as a result of the subsequent deletion of tesB whereas, fatty acid production decreased to 10 mg/L (Fig. 2). As a result of the subsequent tesA deletion, the fatty acid titer decreased to 8 mg/L, whereas the fatty alcohol titer increased to 760 mg/L. Overall, the results demonstrated that the strategy for enhancing fatty alcohol production by inducing fatty acid starvation was effective. Furthermore, the subcellular localization of tesC and the fermentation results suggest that tesC may play the key role in fatty acid formation in E. coli.

Investigating the mechanism of fatty acid starvation by whole-genome transcriptional analysis

To explore the mechanism of enhancing fatty alcohol production with fatty acid starvation, whole-genome transcriptional analysis was performed. Sequence data are available in public databases (NCBI SRA accessions SRA200924). Strains MGKCBA/pL1 and W/pL1 were cultured and collected 12 h after isopropyl β-D-1thiogalactopyranoside (IPTG) induction. The transcription levels of 44 genes in four modules closely related to fatty alcohol production changed (Table 2). (a) The transcription levels of most genes from the glycolysis module were upregulated, particularly ptsG (3.37-fold, p = 0.0023), thus implying that the engineered strain accelerated glycolysis and therefore supplied more precursors for fatty alcohol synthesis (Fig. 1). (b) The transcription levels of most genes from the TCA cycle (except for acnA) were downregulated, particularly sdhA (0.29-fold, p = 0.0031), thus implying that the engineered strain reduced the consumption of the carbon source for cell growth, and this surplus carbon source could then be used for fatty alcohol production. (c) The transcription levels of most genes from the fatty acid synthesis module were upregulated, thereby satisfying the growth demands. (d) The transcription levels of most genes from the fatty acid degradation module were downregulated, particularly fadB (0.36 fold, p = 0.0263), thus implying that the fatty acids produced by the engineered strain

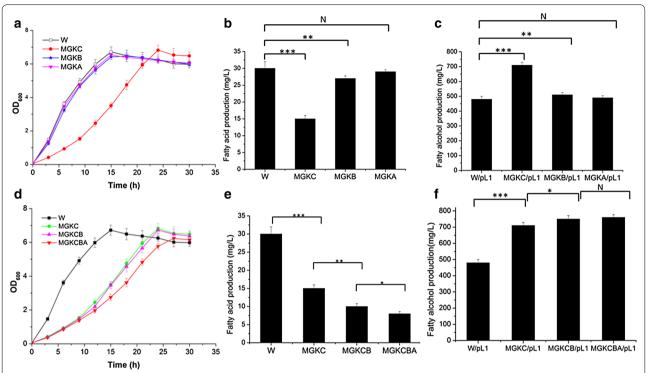


Fig. 2 Fatty alcohol and fatty acid accumulation in engineered strains. The values are the mean of three biological replicates \pm standard deviations (n = 3). **a–c** The growth curves and fatty acid and fatty alcohol production levels in single acyl-ACP thioesterase deletion strains. **d–f** The growth curves, fatty acid production and fatty alcohol production levels in multiple acyl-ACP thioesterase deletion strains. (***) p < 0.001, (**) p < 0.05, (N) p > 0.05, one-way ANOVA. For fatty acid and fatty alcohol production, data were observed 24 h after inoculation in all strains except for MGKCBA/pL1, in which the data were observed 36 h after inoculation

were mainly used to satisfy growth needs, hence, fewer fatty acids were degraded. Moreover, no reads from tesA, tesB or tesC were observed in strain MGKCBA/pL1, thus indicating that these genes were successfully deleted. Additionally, the most highly upregulated gene was ybbO (4.12 fold, p = 0.0131), an NADP⁺-dependent aldehyde reductase that oxidizes alcohol to its corresponding aldehyde. This gene may have assisted in the synthesis of fatty acids from fatty alcohols and partially satisfied the growth need partially. Aside from the deleted genes, the most highly down regulated gene was yibG (0.162 fold, p = 0.0265). However, yibG's function is still unknown [27]. Cell-PLoc 2.0 predicted that the protein encoded by the *yibG* gene is located in cell inner membrane [26]. Blastp analysis of yibG (Domain Enhanced Lookup Time Accelerated BLAST, NCBI) suggested that it might be a tetratricopeptide-like repeat protein, moreover, this protein has been reported to be involved in the stress response via protein-protein interactions [28, 29]. Therefore, *yibG* downregulation may adapt the protein interaction in the *E. coli* inner membrane in response to the induced fatty acid starvation.

In summary, the deletion of acyl-ACP thioesterases resulted in the upregulation of expression of most

genes associated with glycolysis and fatty acid synthesis. This upregulation led to the accumulation of fatty acyl-ACPs, which were finally reduced to fatty alcohols by the expressed FAR (Fig. 1). Furthermore, the downregulation of fatty acid degradation and the TCA module (Table 2) indicated that the designed strategy should be an economic choice for fatty alcohol production. Notably, the transcriptional upregulation of genes from the fatty acid synthesis module was less than 1.67-fold and did not show a statistically significant difference (Table 2). This behavior may be due to the stringent regulation of the fatty acid synthesis pathway. For example, it has been reported that accB acts as an autoregulator of the accBC operon [30], whereas accAD regulates its own translation by binding to the coding region of mRNA for both subunits [28]. Therefore, engineering efforts that focused on key enzymes may be helpful for the further enhancement of fatty alcohol production.

Further improving fatty alcohol production by deleting genes from competing pathways

The MGKCB strain was selected for the subsequent manipulation because it has much shorter fermentation period

Table 2 Transcriptional analysis for genes from the glycometabolism and fatty acid pathway

Gene name	Fold change	p value	Description	Gene name	Fold change	<i>p</i> value	Description
Crr	1.19	0.1422	Glycolysis	рсК	0.75	0.4359	TCA
ptsG	3.37	0.0023	Glycolysis	gltA	0.38	0.0138	TCA
Pgi	2.00	0.0669	Glycolysis	Icd	0.58	0.1293	TCA
pfkB	2.17	0.0687	Glycolysis	sucA	0.49	0.0584	TCA
pfkA	1.52	0.2580	Glycolysis	sucB	0.45	0.0315	TCA
fbaВ	2.72	0.0095	Glycolysis	sucC	0.83	0.6182	TCA
fbaA	1.49	0.3091	Glycolysis	sucD	0.83	0.6182	TCA
gapA	1.22	0.6181	Glycolysis	sdhA	0.29	0.0031	TCA
ytj⊂	1.13	0.8491	Glycolysis	sdhB	0.24	0.0012	TCA
gpmA	1.65	0.1889	Glycolysis	sdhC	0.83	0.0031	TCA
Eno	1.36	0.4461	Glycolysis	sdhD	0.83	0.0031	TCA
pykF	1.34	0.4338	Glycolysis	fumA	0.30	0.0020	TCA
pykA	1.42	0.3519	Glycolysis	fumC	0.66	0.2889	TCA
acnA	1.28	0.4994	TCA	Mdh	0.81	0.5553	TCA
ассА	1.31	0.4684	Fatty acid synthesis	Мдо	0.64	0.2180	TCA
accC	1.48	0.3063	Fatty acid synthesis	fadD	0.66	0.2633	Fatty acid degradation
accD	1.39	0.3625	Fatty acid synthesis	fadE	0.58	0.1408	Fatty acid degradation
fabD	1.58	0.2078	Fatty acid synthesis	fadB	0.36	0.0263	Fatty acid degradation
fabH	1.58	0.2090	Fatty acid synthesis	fadJ	0.82	0.6126	Fatty acid degradation
fabB	1.17	0.6594	Fatty acid synthesis	fadA	0.54	0.1024	Fatty acid degradation
fabG	1.41	0.3477	Fatty acid synthesis	fadl	0.82	0.6126	Fatty acid degradation
fabZ	1.67	0.1716	Fatty acid synthesis	yqeF	0.37	0.0175	Fatty acid degradation

Genes with fold-change value >1.1 and <0.9 are shown

but a similar fatty alcohol production, as compared with MGKCBA/pL1 strain. To enhance fatty alcohol production, deletions of lactate dehydrogenase (*ldhA*), acetate kinase (*ackA*) and phosphate acetyltransferase (*pta*) were performed, resulting in the MGL2 strain. As shown in Fig. 3a, b, the highest optical density at 600 nm (OD₆₀₀) was increased from 5.2 to 7.8. Moreover, the fatty alcohol titer increased from 756 to 2024 mg/L (Fig. 3a–c). The deletions of *ldhA*, *pta* and *ackA* dramatically decreased the production of lactate (from 0.1 to 0.06 g/L) and acetate (from 4.9 to 1.1 g/L) (Fig. 3d, e). Fatty alcohol productivity reached 259 mg/OD/L in the MGL2 strain, which is about approximately 1.7-fold higher than that of the MGKCB/pL1 strain.

The distribution of fatty alcohols produced by the MGL2 strain ranged from C12 to C18 (Fig. 3f), similarly to previously reported results [16]. MGL2 predominantly produced two saturated (C14:0 and C16:0) and two unsaturated (C16:1 and C18:1) fatty alcohols. The two major products, C14:0 and C16:1, accounted for 35.6 and 30.8 % of the total fatty alcohol production, respectively. Notably, this reported titer was achieved in MGL2 under shake flask fermentation for only 24 h. These results suggest that blocking fatty acid formation coupled with deleting competing pathways for acetyl-CoA pool efficiently enhanced fatty alcohol production.

Fatty alcohol production by fed-batch fermentation

Fed-batch fermentations were performed using fermentation medium in 3-L Bioflo 110 with MGL2 strain. The total fatty alcohol accumulation reached a maximum titer of 6.33 g/L at 50 h, At which point, the OD₆₀₀ reached 46 (Fig. 4a). Both the cell density and the fatty alcohol concentration stopped increasing after 50 h. Notably, the fatty acid concentration was lower than 12 mg/L during the entire fermentation process (Fig. 4a). Thus, the high fatty alcohol titer could be partly attributed to fatty acid starvation during fermentation. The fatty alcohol composition produced in MGL2 under fed-batch fermentation (Fig. 4b) was similar to that of shake-flask fermentation: two saturated (C14:0 and C16:0) and two unsaturated (C16:1 and C18:1) fatty alcohols were the major components. The percentage of unsaturated fatty alcohols reached up to 36.5 % of the total fatty alcohols (Fig. 4b). Additionally, the fed-batch fermentation with strain MGL2 was conducted in M9 medium with glycerol as the only carbon source. The final titer was 5.94 g/L (data not shown), which was also higher than any previously reported values. The results above demonstrated that our strategies might be useful in the industrial production of fatty alcohols.

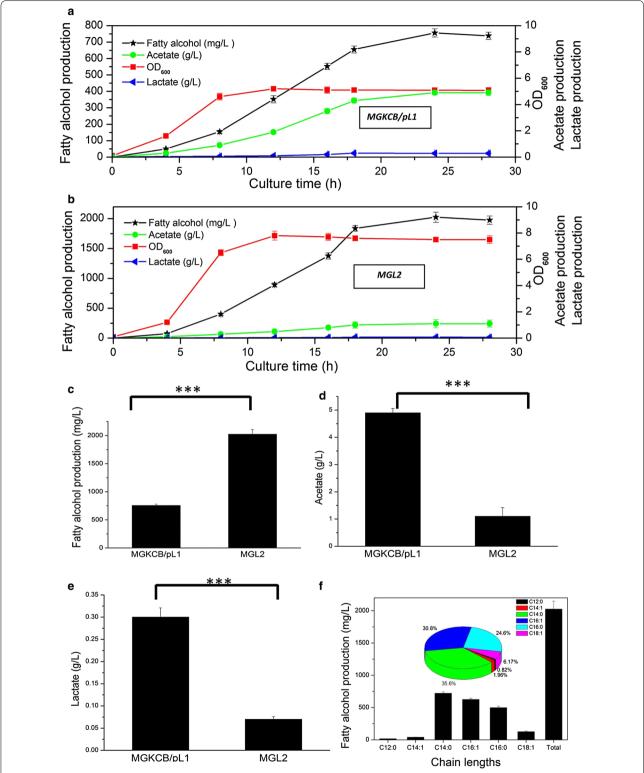
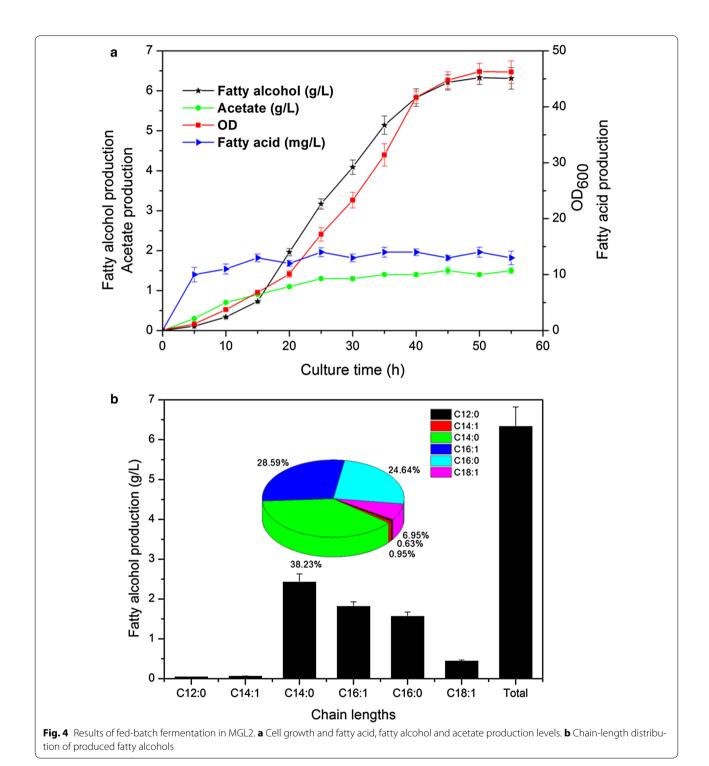


Fig. 3 The effects of deleting genes from competing pathways on fermentation. **a** Fermentation results for MGKCB/pL1. **b** Fermentation results for MGL2. **c** Comparison of fatty alcohol production between MGKCB/pL1 and MGL2 strains. **d** Comparison of acetate accumulation between MGKCB/pL1 and MGL2 strains. **e** Comparison of lactate accumulation between MGKCB/pL1 and MGL2 strains. **f** Distribution of fatty alcohols with different carbon chain lengths in MGL2. The values are the means of three biological replicates. (***) p < 0.001, one-way ANOVA. **c-f**, data were observed 24 h after inoculation



Investigation of the toxicity and cellular localization of fatty alcohols

Toxicity is vital for the microbial production of chemicals because physiological investigation has revealed a correlation between solvent toxicity to microbes and the logP value [31, 32], which has been defined as the partition

coefficient of the given solvent in an equimolar mixture of octanol and water [33]. The lower the logP value, the higher the toxicity of the solvent [31]. Among the fatty alcohols produced, dodecanol have the lowest logP value and is supposed to have the highest toxicity. Hence, the toxicity of dodecanol to *E. coli* was analyzed. Figure 5

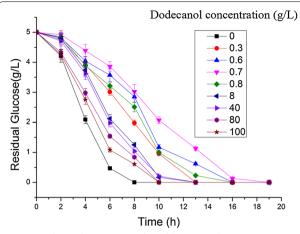


Fig. 5 Dodecanol toxicity test. The wild-type *E. coli* MG1655 strain was cultured in LB medium with 5 g/L of glucose. Dodecanol was added in concentration ranging from 0 to 100 g/L. The values are the means of three biological replicates

shows that, when the dodecanol concentration increased from 0 to 0.7 g/L, the toxicity increased simultaneously. As its concentration increased thereafter, the toxicity of dodecanol decreased, possibly because when the concentration was relatively low, the small droplets of dodecanol attached to the cell membranes and affected the mass transfer, thereby harming to cells. When the concentration became relatively higher, the small droplets of dodecanol might have adhered to each other instead, thus reducing the solvent's toxicity to cells. These results suggested that overproduction of fatty alcohols in *E. coli* may be possible.

Cellular localization is also important for microbial productions. Intracellular products are limited by the maximum biomass, while the situation is different for extracellular products. The cellular localization of produced fatty alcohols was investigated via in situ product separation tests in the W/pL1 and MGL2 strains. As shown in Additional file 1: Table S1, the produced fatty alcohols were detected in the tridecanol layer, whereas, no fatty alcohol was detected in the medium or the cells. Thus, fatty alcohols produced in E. coli are extracellular products and will not be limited by the maximum biomass. Interestingly, the output of fatty alcohols in the in situ separation fermentation was slightly higher than that in the control, possibly because the produced fatty alcohols attached to cell membranes without the addition of extraction solvent, thus affecting mass transfer and fatty alcohol production. Notably, in the control test the fatty alcohols produced in strain W/pL1 adhered to cells after centrifugation, whereas the situation was different in MGL2. These results supported our speculation that fatty alcohol droplets at low concentration will attach tocells but instead attach to each other and are suspended in the medium after their concentration increase beyond a certain threshold.

Conclusions

In summary, a fatty alcohol titer of 6.33 g/L was achieved in fed-batch fermentation in *E. coli* via the deletion of fatty acyl-CoA thioestarase, to starve cells of fatty acids, as well as deletion of *ldhA*, *pta* and *ackA* from competing pathways. Moreover, fatty alcohols were shown to be extracellular products with low toxicity to *E. coli*. These results indicate a bright future for microbial production of fatty alcohols.

Methods

Materials

Restriction enzymes and T4 ligase were purchased from Takara Biotechnology (Dalian, China). PCR purification kits, gel extraction kits, QIAprep Spin plasmid miniprep kits, were from Axygen (Union City, CA, USA). Oligonucleotide primers were synthesized by Sangon Biotechnology (Shanghai, China) (Additional file 1: Table S2). Fatty acid standards were purchased from Nu-Check-Prep (Elysian, MN, USA). Fatty alcohol standards were purchased from Dr. Ehrenstorfer GmbH (Augsburg, Germany).

Bacterial strains and plasmid construction

All bacterial strains and plasmids used in this work are listed in Table 1. All deletions were performed with our recently developed method [8]. First, fragments containing cat-sacB flanked by tandem repeats were constructed with primers (Additional file 1: Table S2) and then introduced into the target site via intermolecular homologous recombination assisted by lambda red enzymes (pKD46). Then, recombinants were selected from Luria-Mertani (LB) agar plate containing chloramphenicol (34 mg/L). Seamless excision of the selectable marker was achieved using sucrose [8]. The FAR gene (maqu_2220) was amplified from M. aquaeolei VT8 DNA by PCR using the primers FARF and FARR. The PCR product was purified and digested with BamHI and EcoRI. After purification, the digested PCR fragment was cloned into the expression vector pTrcHisA, resulting in the recombinant plasmid pL1. E. coli MG1655 was used as the original strain.

Culture conditions

LB medium was used to assess the effects of gene deletions on cell growth. To assess fatty alcohol production by different engineered $E.\ coli$ strains, three single colonies of each strain were cultivated in LB medium containing 100 µg/mL ampicillin overnight at 37 °C. Each seed culture was inoculated into 50 mL of LB containing a mixed

carbon source (0.5 % glucose, 2.5 % glycerol) in a 250-mL flask, and this was followed by incubation at 37 °C and 220 rpm. When the $\rm OD_{600}$ reached 0.6–0.8, IPTG was added to a final concentration of 0.2 mM. 5-mL cell culture was used for fatty alcohol analysis.

Fed-batch fermentation was performed with a medium volume of 1 L in a 3-L Bioflo 110 fermentor (New Brunswick Scientific, Edison, NJ, USA). Strains were cultivated in 40 mL of seed medium (5 g/L yeast extract, 10 g/L tryptone, 10 g/L glycerol) in a 250-mL flask containing 100 μg/mL of ampicillin overnight at 37 °C. The seed culture was inoculated into 1 L fermentation medium (10 g/L yeast extract, 20 g/L tryptone, 25 g/L glycerol, 3 g/L KH₂PO4, 8 g/L Na₂HPO₄·12H₂O, 0.2 g/L CaCl₂, 100 μg/mL ampicillin, 1 mM MgSO₄, 100 μg/mL ampicillin). When the OD₆₀₀ reached 0.6-0.8, IPTG was added to a final concentration of 0.2 mM. The temperature was maintained at 37 °C, and the pH was kept at 7.00 by the addition of 25 % (v/v) NH_4OH or 1 M HCl solutions. A constant glycerol feed-rate of 0.5 g/h was maintained. Agitation was provided by a single impeller with the stirring speed set between 200 and 500 rpm. The stirring speed was controlled to ensure that the dissolved oxygen (DO₂) content was greater than 10 %. The air inflow rate was maintained at 3.0 L/min.

To assess the toxicity of fatty alcohol to *E. coli*, the original strain was cultured in LB medium containing 5 g/L glucose and dodecanol in different concentrations ranging from 0 to 100 g/L. Because the addition of dodecanol affects the quantitative measurement of biomass, the consumption of glucose and not biomass was analyzed to assess the toxicity. To investigate the location of produced fatty alcohols, in situ product separation tests were conducted in strains W/pL1 and MGL2. Colonies of each strain were cultured in LB medium containing 100 µg/ mL of ampicillin overnight at 37 °C. The seed culture was inoculated into 50 mL of LB medium containing 2.5 % glycerol in a 250-mL flask at 37 °C and 220 rpm. When the OD_{600} reached 0.6–0.8, 0.2 mM IPTG was added. Tridecanol was used as an extraction solvent and added to the medium before inoculation. The solvent to sample ratio is 1:5. Medium without tridecanol was used as control.

Analytic methods

The bacterial growth conditions were estimated from the ${\rm OD}_{600}$ of the medium with a spectrophotometer (723 N, Shanghai Precision & Scientific Instrument Co. Ltd, China). The concentrations of glucose, glycerol, lactate and acetate were analyzed by high-performance liquid chromatography (HPLC) with an Agilent1200 (Agilent, Co. Ltd USA) equipped with UV absorbance and refractive index detectors (RID) and a Bio-Rad Aminex

HPX-87H column (300 \times 7.8 mm). The mobile phase was 5 mmol/L H_2SO_4 , The flow rate was 0.6 mL/min, and the column temperature was 50 °C. Culture broth was centrifuged at 10,000 rpm for 10 min, and 10 μL of the diluted sample was injected into the HPLC instrument.

The analysis of fatty acids and fatty alcohols was performed via HPLC with an Agilent 1200 (Agilent, Co. Ltd. USA) equipped with RID and a SilGreen ODS C18 column (4.6 mm \times 250 mm, 5 μ m) according to the reported research [34]. The mobile phase was methanol: water: acetic acid (90:9.9:0.1, v/v/v). The column temperature was 26 °C with a flow rate of 1.0 mL/min. Fivemilliliter samples of fermentation combined with 500 µL of 10 mol/L HCl were extracted with 2.5 mL of ethyl acetate at 10 °C and 260 rpm for 2 min. The mixtures were shaken vigorously for a few seconds before they were placed in a rotary shaker incubator. After extraction, the mixtures were left static for 10 min and the organic layer was then transferred to a new centrifuge tube. After centrifugation at 12,000 rpm for 5 min, the clear supernatant was collected and filtered through a 0.45-µm millipore filter and injected into the HPLC-RID system for analysis.

Whole-genome transcriptional analysis

Three replicates of the fatty alcohol-overproducing strain MGKCBA/pL1 and three replicates of the control strain W/pL1 were cultured in modified LB medium as described above. Cells of the two genotypes were mixed separately after 12 h of induction with IPTG and were harvested by quick centrifugation (at 10,000g, 4 °C for 1 min) and then immediately frozen in liquid nitrogen. Total RNA was extracted using an RNeasy Mini kit (Qiagen, Valencia, CA, USA) following lysozyme treatment. The total RNA in each sample was quantified and qualified with an Agilent 2100 Bioanalyzer (Agilent Technologies). Pair-end (PE) index libraries were constructed according to the manufacturer's protocol (NEBNext® Ultra[™] Directional RNA Library Prep Kit for Illumina[®]). Sequencing was performed using a 2×100 PE configuration. Image analysis and base calling were conducted by the HiSeq Control Software (HCS) + OLB + GAPipeline-1.6 (Illumina) in the HiSeq instrument. The sequences were processed and analyzed by GENEWIZ (Suzhou, China). More information can be found in Additional file 1: Method S1.

Additional file

Additional file 1. Additional information.

Authors' contributions

YLL designed experiments and performed experiments and prepared the manuscript. MHY, JMZ and YYW performed experiments and drafted the

manuscript. SC, XNQ and JJC designed experiments and helped to revise the manuscript. JMX, QHW and YHM designed experiments and prepared the manuscript. All authors read and approved the final manuscript.

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Competing interests

The authors declare that they have no competing interests.

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